

Review of experimental measurements involving dd reactions

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Presented at the Short Course on LENR for ICCF-10
August 25, 2003

Outline

1. Contributors
2. How this all started?
3. Issues of Pd/D Loading
4. Calorimetric results
5. Nuclear effects
6. Conclusions

Primary Contributors and Collaborators

- SRI Staff: B. Bush, S. Crouch-Baker, N. Jevtic, A. Hauser, A. Riley, R. Rocha-Filho, S. Smedley, **F. Tanzella**, R. Weaver, S. Wing
- Consultants: W. B. Clarke, L. Case, R. George, B. Oliver, K. Wolf
- EPRI: J. Chao, T. Passell, J. Santucci, M. Schreiber
- Lockheed: J. Pronko, D. Kohler
- ENEA (Frascati): P. Tripodi, V. Violante
- MIT: **P. Hagelstein**, L. Smullin
- NRL: **G. Hubler**
- U of Strathclyde: L. Berlouis, P. Honner, F. McMahon, M. Taylor, A. Wark,
- Project Cobalt: K. Mullican, M. Trevithick
- Osaka Univ.: Y. Arata, Y. Zhang

Low temperature nuclear activity in solids

The recent phase of attention was stimulated by two publications in 1989:

Fleischmann and Pons:

Principal claim is excess heat from Pd cathode electrolyzed in heavy water

Jones *et al*:

Neutrons claimed as evidence of low-level dd-fusion reactions from Ti cathode electrolyzed in heavy water

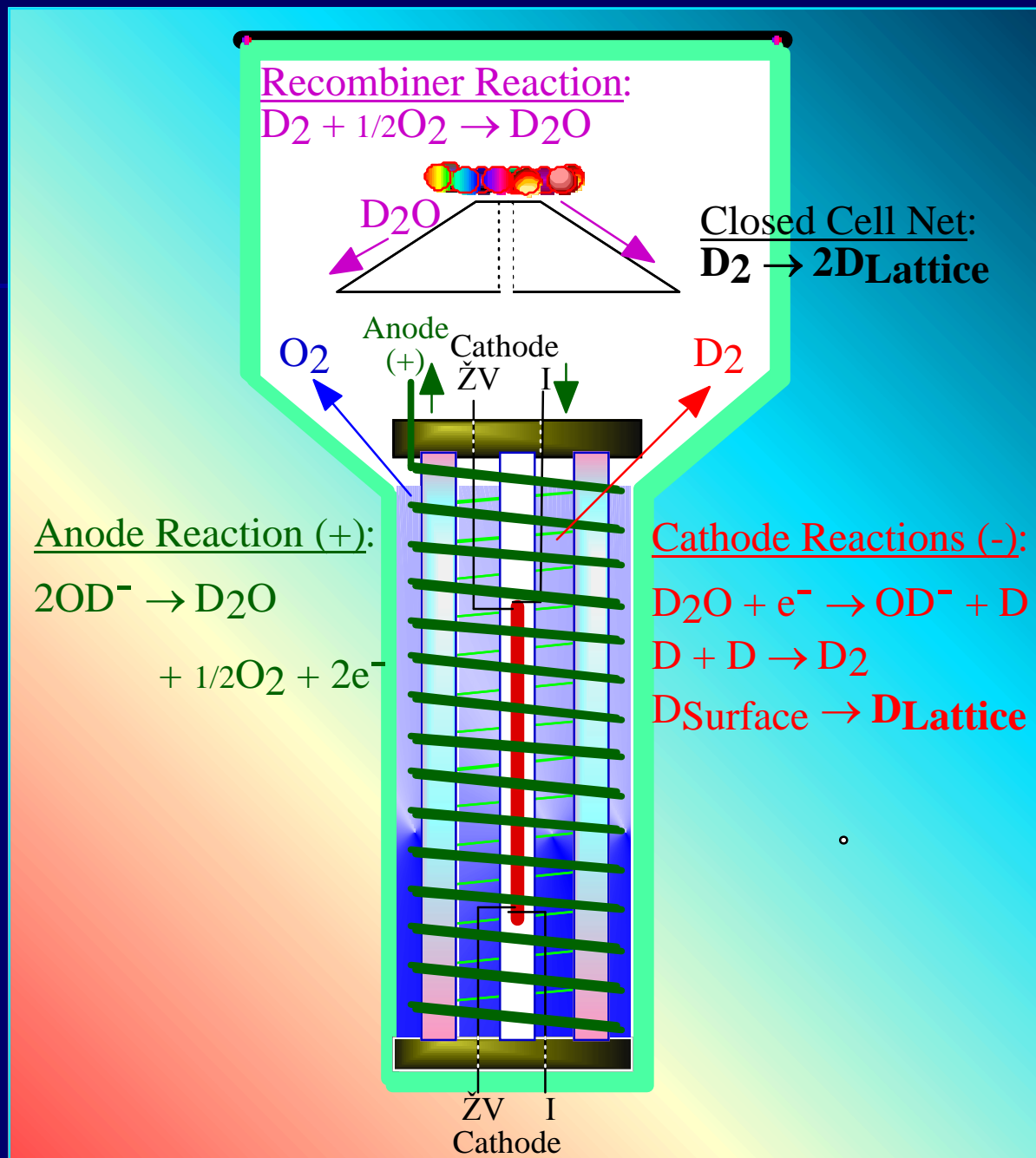
Hypothesis 1

“There is an unexpected and unexplained source of heat in the D/Pd System that may be observed when Deuterium is loaded electrochemically into the Palladium Lattice, to a sufficient degree.”

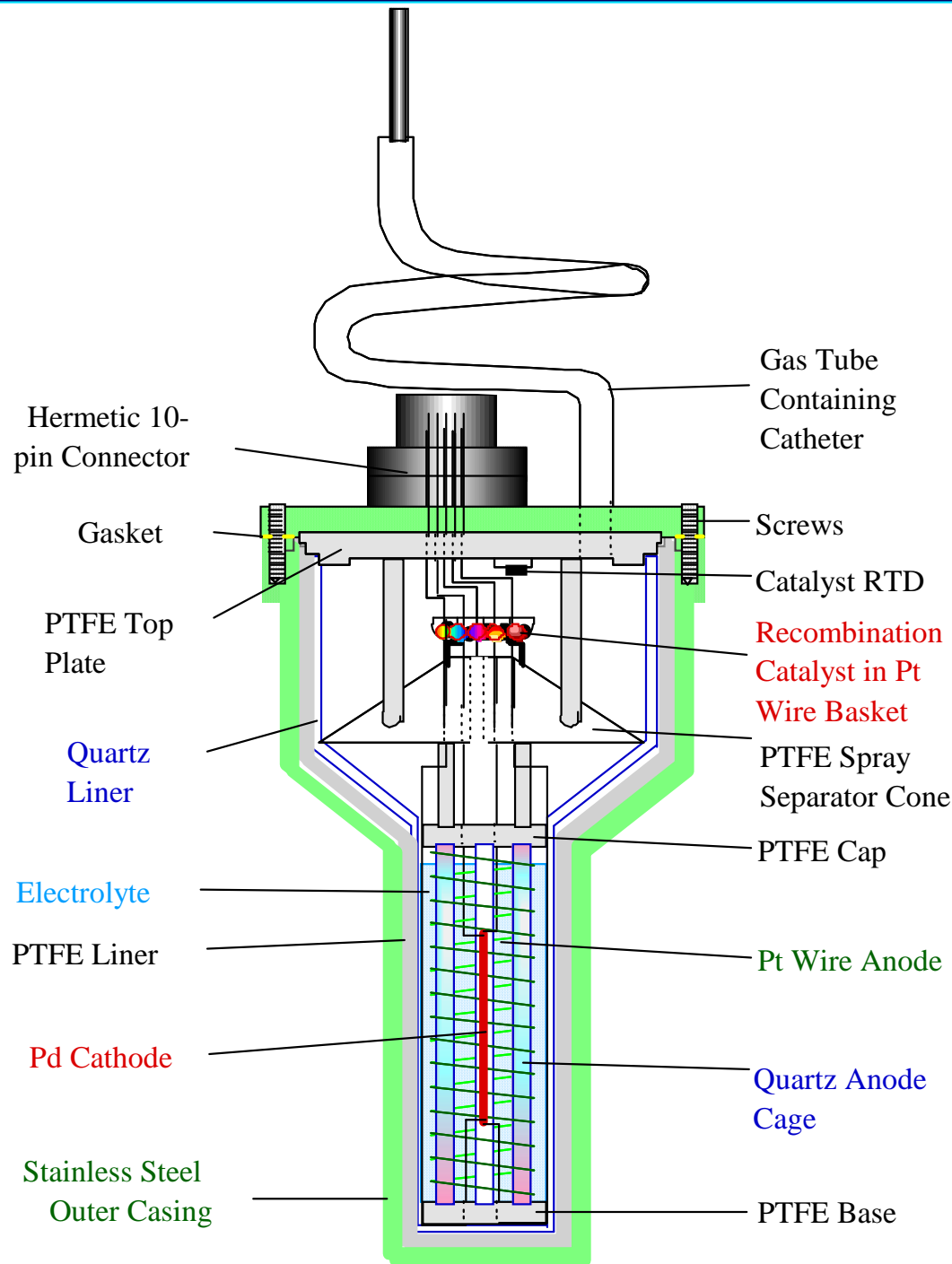
Experiments:

- D/Pd Loading studies (R/R° , interfacial Z).
 - Electrochemical Impedance (kinetics & mechanism)
 - Resistance Ratio (extent of loading)
- Calorimetry
 - first principles closed-cell, mass-flow calorimeter,
 - > 98% heat recovery
 - absolute accuracy < $\pm 0.4\%$

Electro-chemical Loading of Pd in a Thermodynamically Closed Cell:



SRI Quartz Calorimeter and DoL Cell



Requirements of a (CF) Calorimeter (1989)

Conceptually simple system based on first principles

Maintain control of operating parameters (including T_{Cell})

On-line monitoring of all relevant variables **including D/Pd**

Multiply redundant measurement of parameters
critical to calorimetry

Accommodate large dynamic range of P_{in} and P_{out} (0.1 - 100W)

Closed and isolated electrochemical system to retain all products

High accuracy and precision (< 1 ppt)

Known sources of systematic error yield conservative estimates
of output heat

Flow Calorimetry (1989): Advantages

All the heat evolved by electrochemical cell is absorbed by the heat transfer fluid

Control temperature of electrochemical cell by controlling heat transfer fluid flow rate and temperature

Can accommodate large inputs of electrochemical power and large dynamic range of heat input and output

Calibration not required

Flow Calorimetry (1989): Potential Problems

Flow rate must be measured on-line for high accuracy

Calibration desirable for high accuracy

Flow streamlining at points of temperature measurement can lead to errors

Heat Relationships

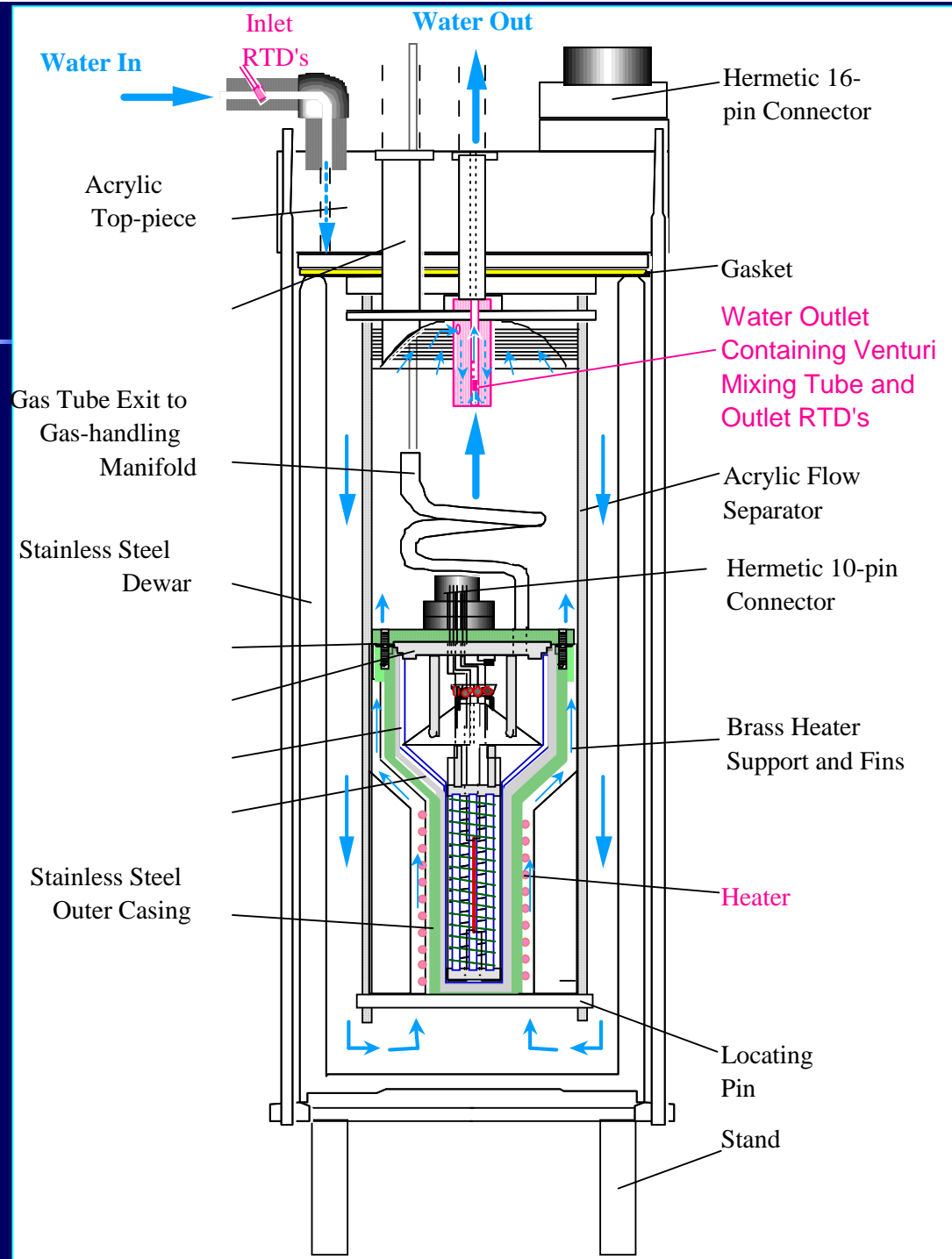
$$P_{\text{heater}} + P_{\text{electrochem}} = (C_p \delta m / \delta t + k') (T_{\text{out}} - T_{\text{in}})$$

C_p = heat capacity of heat transfer fluid

$\delta m / \delta t$ = mass flow rate

k' = effective heat loss constant

T_{in} and T_{out} are inlet and outlet sensor temperatures



SRI LL Calorimeter and Cell

<i>First 25</i>				Electrolyte:		T	P	Max. I:		Min.	Max.	Expt Init.		P _{xs}		Inpu	Output-Input											
Pd	l	d	A	mM	Conc.	Add.	°C	(psi)	A /	cm ²	R/R°	D/Pd	(h)	(h)	(W)	%	MJ	MJ	%	eV	#							
<u>Differential Calorimeter</u>													<i>(High pressure, Low temperature)</i>															
													<i>2.2 Years</i>															
P1a	AECL	5.0	0.7	11	217	LiOD	1.0	none	7	650	7.5	0.68	1.20	1+	696	369	1.8	52%	3.4	0.07	2.1%	3.4	5					
P1b	*	5.0	0.7	11	4E-4	LiOD	1.0	none	7	650	7.5	0.68	Cu Substr.		696	299	0.2	7%		0.01		4.E+05	2					
<u>P2 Series (High pressure flow Calorimeter)</u>																												
P2	Engel.	4.5	0.3	4.2	36	LiOD	1.0	none	4	1000	2.1	0.50	1.65	0.95	1393	504	2.0	53%	50	1.07	2.1%	310	4					
P3	Engel.	4.5	0.3	4.2	36	LiOD	1.0	none	4	1000	1.5	0.35	1.70	0.90	1250				18									
P7	Engel.	4.5	0.3	4.2	36	LiOD	1.0	none	8	1000	1.1	0.26	Contact Prob.		145				2.1									
P10	Engel.	4.5	0.3	4.2	36	LiOD	1.0	none	35	900	0.2	0.05	Contact Prob.		18				0.3									
P11	Engel.	4.5	0.3	4.2	36	LiOD	1.0	none	35	1050	5.0	1.18	1.65	0.95	85				1.2									
<u>P4 Series (Medium Pressure)</u>																												
P4	Engel.	5.0	0.3	4.7	40	LiOD	0.1	none	15	100	2.4	0.51	1.80	0.80	1165				17									
P5	Engel.	5.0	0.3	4.7	40	Li ₂ SO ₄	0.5	none	16	100	4.0	0.85	1.70	0.90	287				4.1									
P6	Engel.	5.0	0.3	4.7	40	Li ₂ SO ₄	0.5	As ₂ O ₃	8	100	2.7	0.57	1.70	0.90	649				9.3									
P8	Engel.	3.0	0.3	2.8	24	LiOD	0.1	none	15	100	1.8	0.64	1.65	0.95	186				2.7									
P9	Engel.	3.0	0.3	2.8	24	LiOD	1.0	none	35	50	1.5	0.53	1.65	0.95	597				22									
<u>P12 Series (Al & Si)</u>																												
P12	Engel.	3.0	0.3	2.8	24	LiOD	1.0	⁴He,Al	30	50	2.5	0.88	1.55	0.98	1631	316	1.0	10%	59	0.80	1.4%	346	4					
P13	Engel.	3.0	0.3	2.8	24	LiOH	1.0	Al	30	50	2.5	0.88	1.1*	0.98	815				12									
P14	Engel.	3.0	0.3	2.8	24	LiOD	1.0	³He,Al	30	50	2.5	0.88	1.60	0.94	692	184	0.5	5%	10	0.20	2.0%	84	2					
P15	Engel.	3.0	0.3	2.8	24	LiOD	1.0	Al	35	40	2.5	0.88	1.58	0.97	1104	684	2.4	24%	40	0.55	1.4%	238	3					
P16	Engel.	3.0	0.3	2.8	24	LiOD	1.0	³He,Al	35	40	2.5	0.88	1.70	0.90	1104	948	0.4	4%	40	0.10	0.2%	42	4					
P17	Engel.	3.0	0.3	2.8	24	LiOD	1.0	Si	29	40	1.1	0.39	1.29	1+	1202	1040	0.2	2%	13	0.10	0.7%	42	2					
P18	Engel.	3.0	0.3	2.8	24	LiOD	1.0		35	40	Failed early due to electrical contact																	
P20	Engel.	3.0	0.3	2.8	24	LiOD	1.0	Al	35	40	2.0	0.71	1.55	0.98	954	650	0.3	2%	17	0.16	1.0%	71	3					
<u>P19 Series (Boron)</u>																												
				Outlet; 2 RTD & 2 thermistors								B effect, multi-humped R response																
P19	Engel.	3.0	0.3	2.8	24	LiOD	1.0	B	35	40	1.9	0.67	1.45	0.99	1287	261	0.9	340%	23	0.41	1.8%	180	4					
P21	Engel.	3.0	0.3	2.8	24	LiOD	1.0	B	30	40	2.0	0.71	1.60	0.94	764	390	0.6	6%	14	0.04	0.3%	17	2					
P22	Engel.	3.0	0.3	2.8	24	LiOD	1.0	B	30	40	2.0	0.71	1.30	1+	1480	378	0.1	30%	21	0.27	1.3%	119	3*					
<u>C Series (Large Area)</u>													Last event terminated by H ₂ O addition *															
C1	JM	30	0.1	9.4	27	LiOD	1.0	Al	30	50	7.2	0.76	1.65	0.93	866	390	1.4	3%	49	1.12	2.3%	437	1					
C2	JM foil	25	μm	60	3	LiOD	1.0	Al	30	50	7.2	0.12	1.60	0.94	356	190	3.0	10%	14	0.56	3.9%	2076	1					

SRI
First
25

Excess Power vs. Maximum Loading (1)

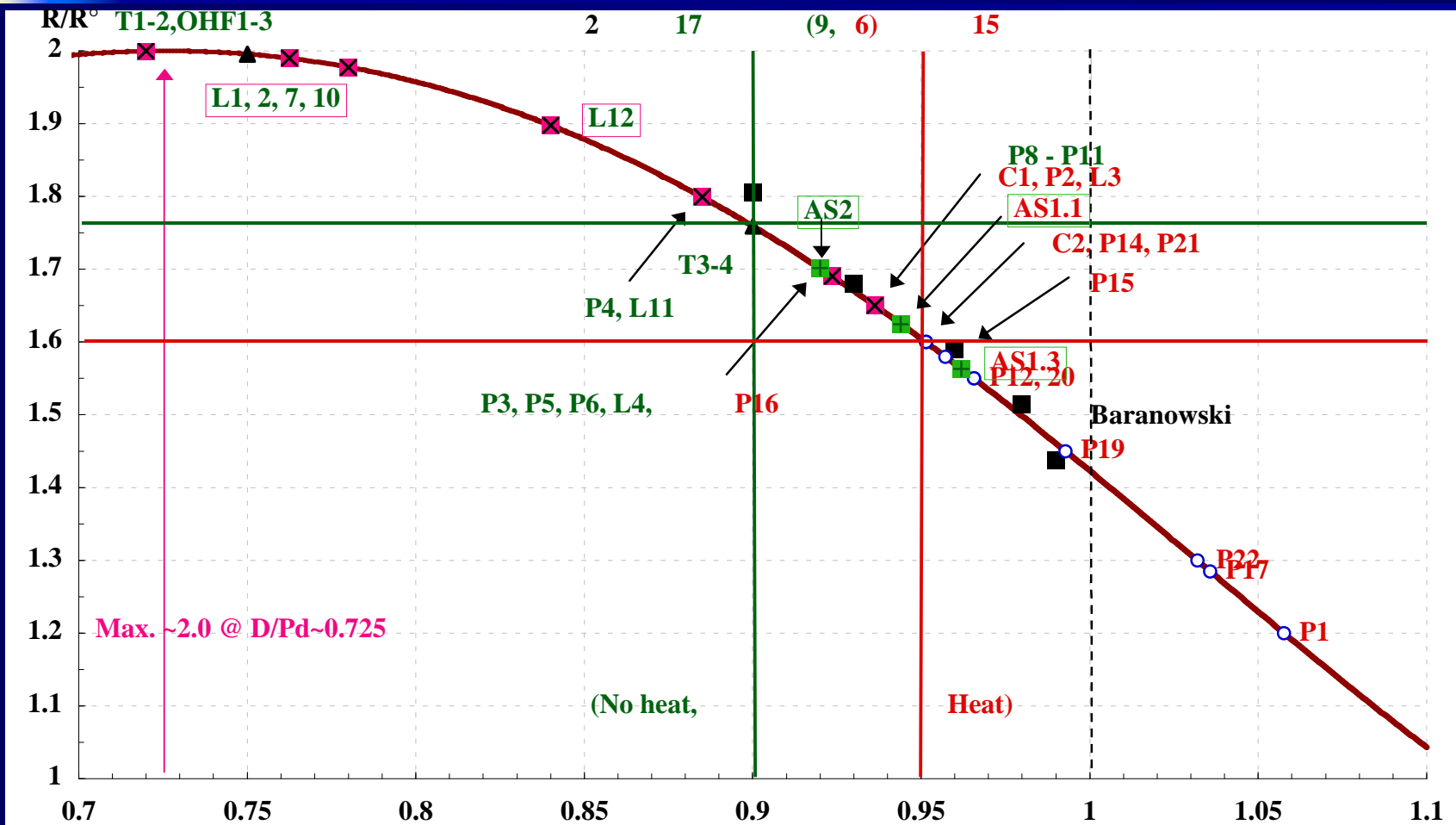
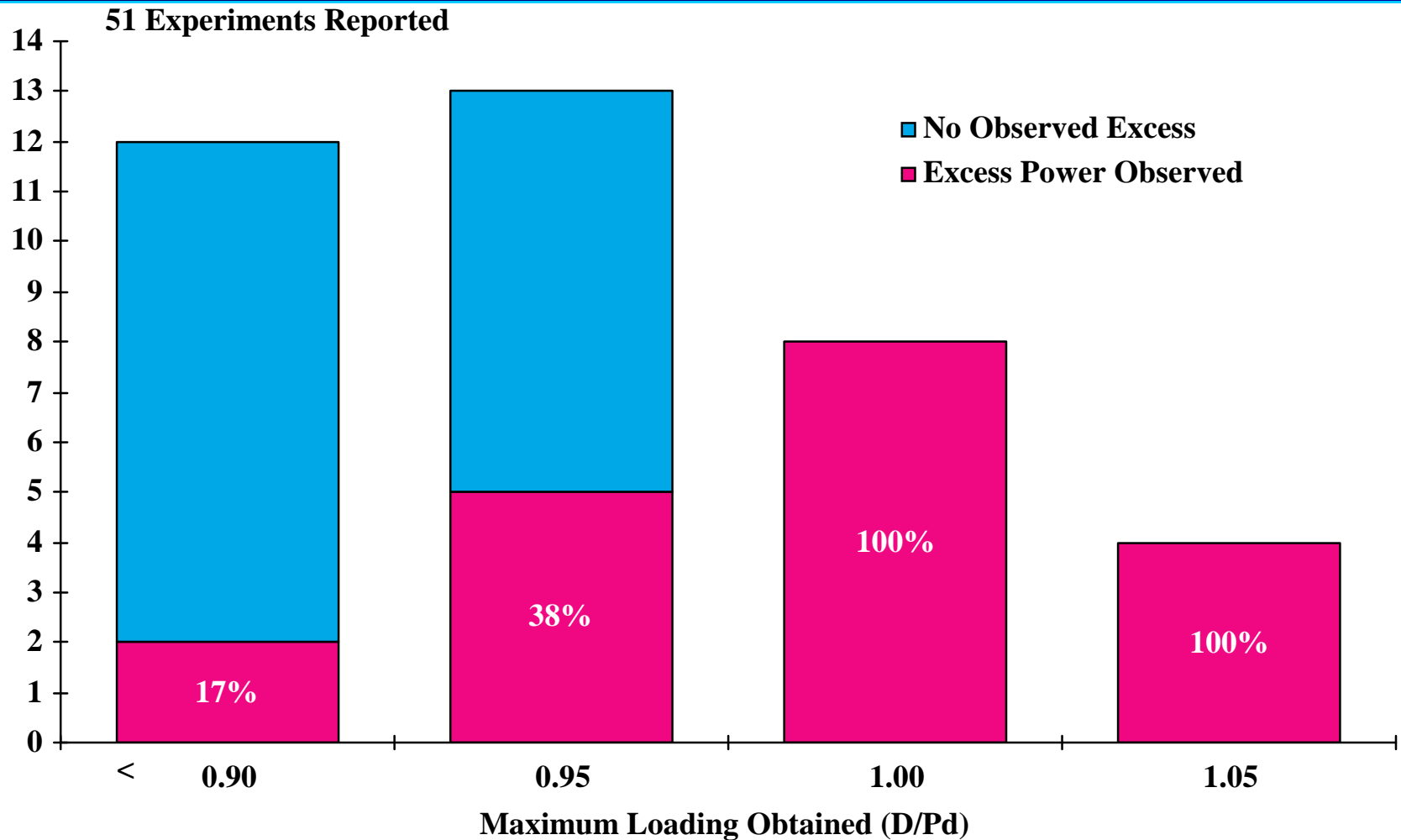
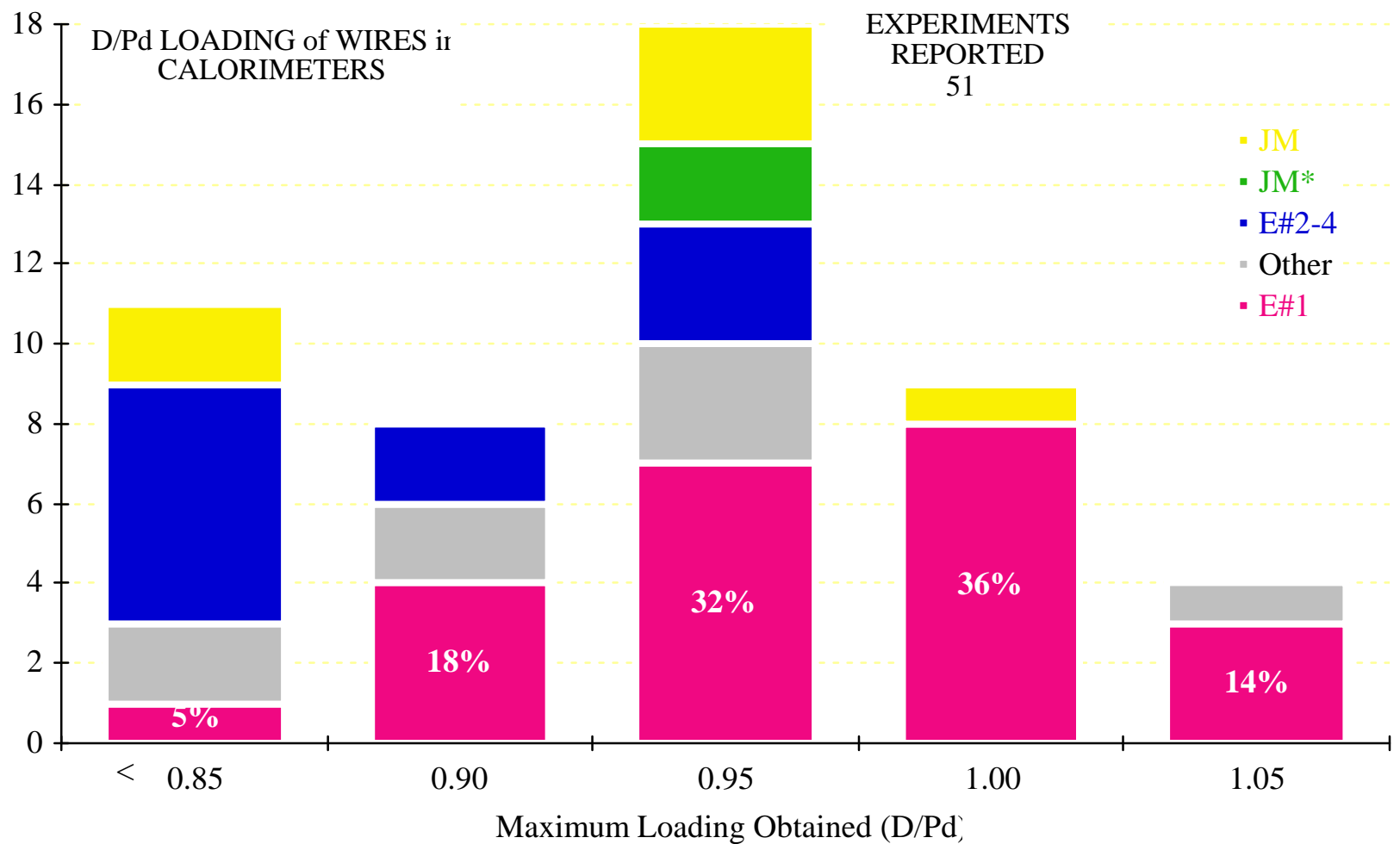


Figure 1 Maximum loading, D/Pd , attained in experiment; determined by R/R° .

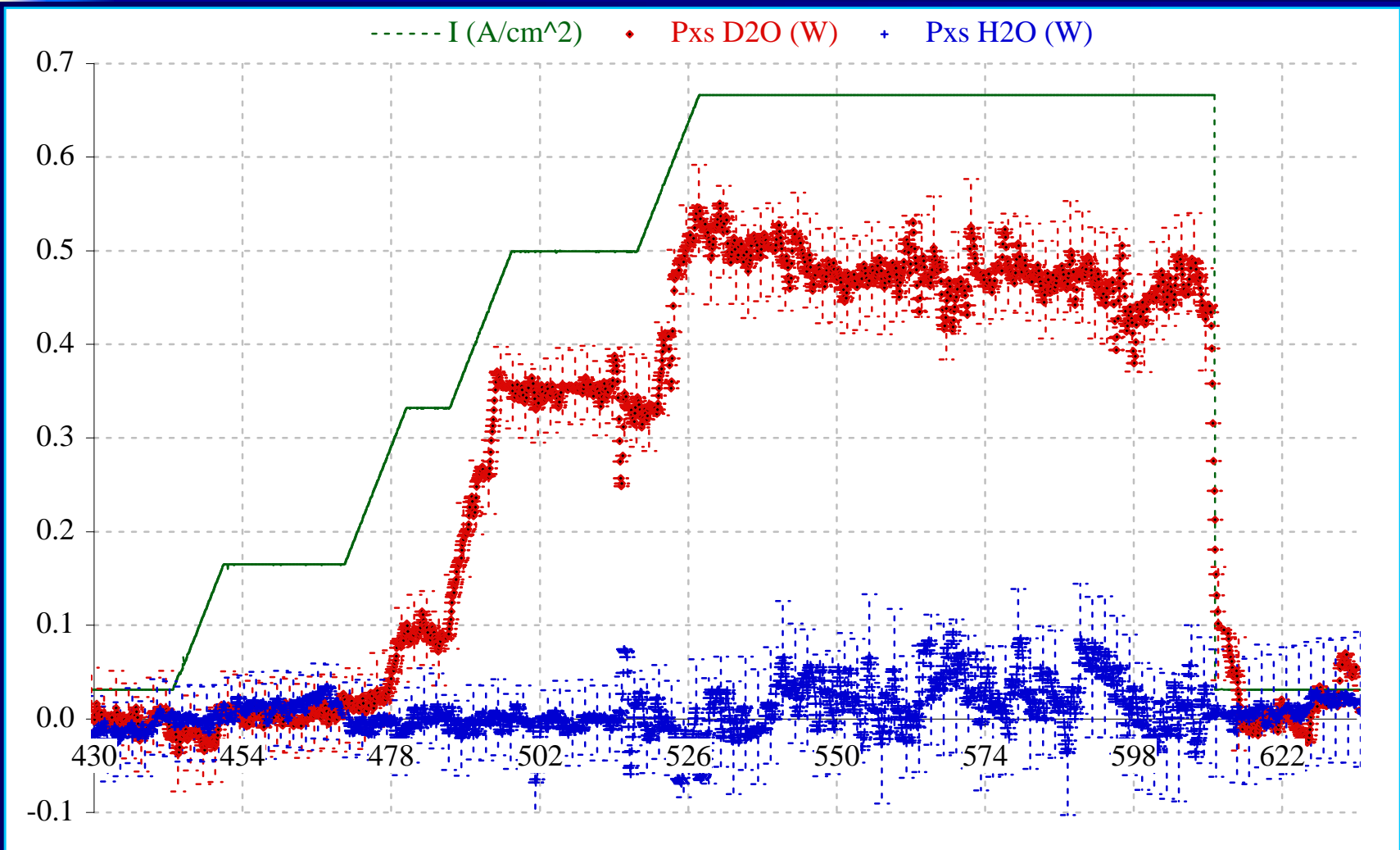
Excess Power vs. Maximum Loading (2)



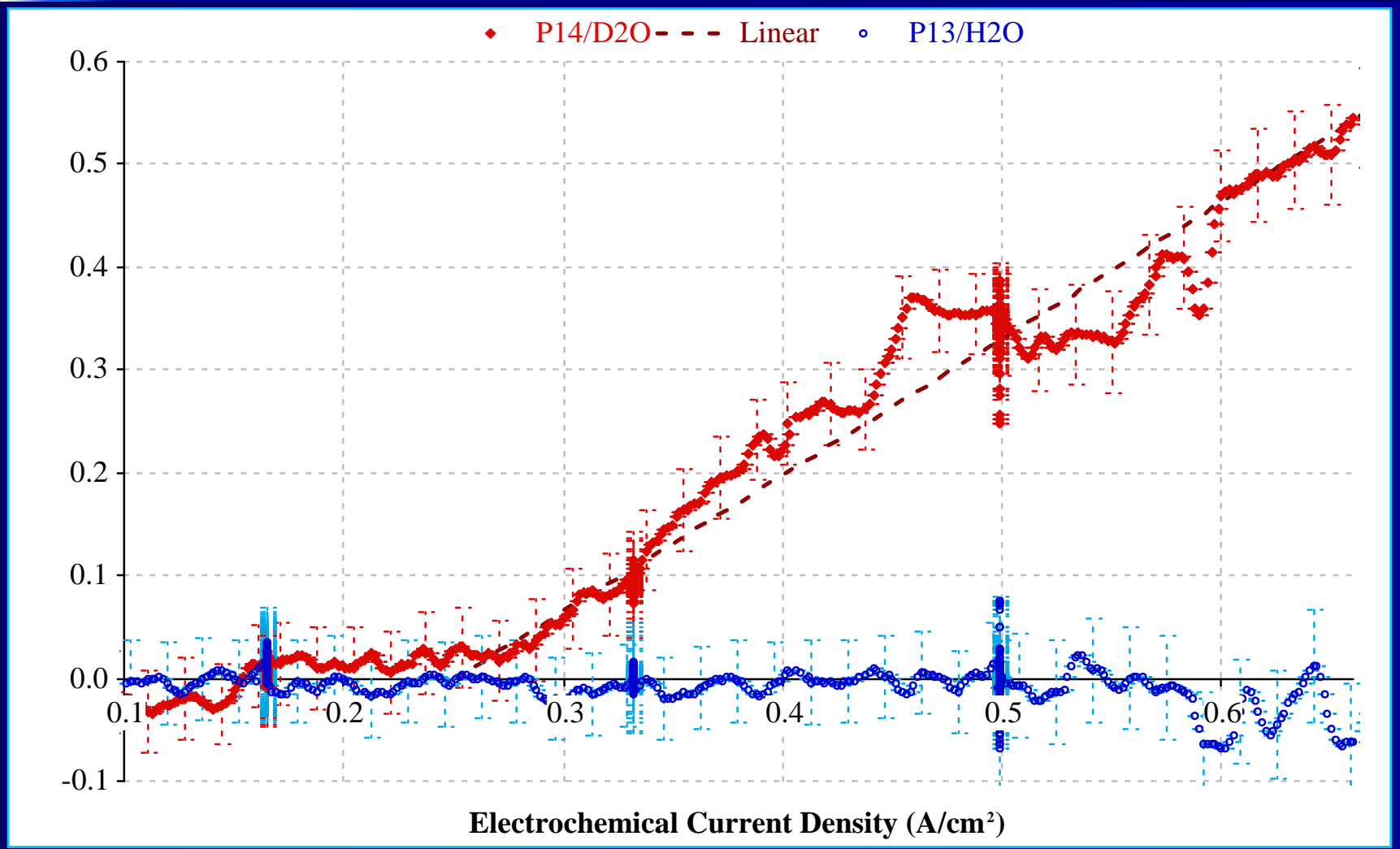
Excess Power vs. Palladium Source



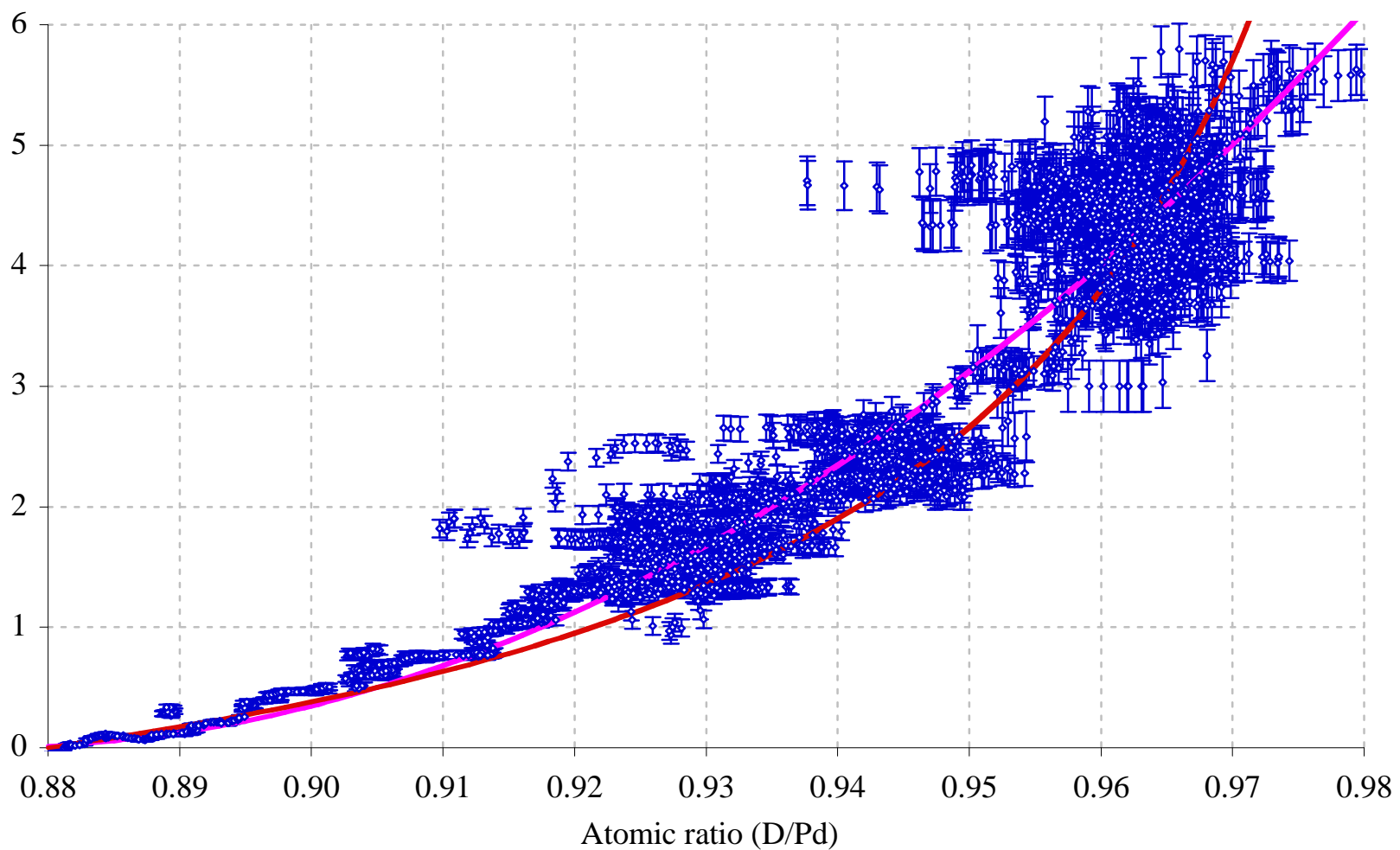
P13/14 Simultaneous Series Operation of Light & Heavy Water Cells; *Excess Power & Current Density vs. Time*



P13/14 Simultaneous Series Operation of Light & Heavy Water Cells; *Excess Power vs. Current Density*



C1: Excess Power vs. D/Pd



Conclusions regarding Excess Heat Production in Bulk Pd Cathodes Electrolytically Loaded with D:

- Effect Evidenced on numerous occasions (**>50**)
- Typical P_{xs} 3 - 30% ($\pm 0.5\%$) of Total P_{in} (**340%**)
- Up to 90σ observation of excess power effect
- Duration several hours to 1 week
- 100's to 1000's of eV's / Pd (D) atom (**2076**)
- Sustained, unidirectional heat burst exhibit an integrated energy at least 10x greater than the sum of all possible chemical reactions within a closed cell
- Heat effects are observed with D, but not H, under similar (or more extreme) conditions

Necessary Conditions for Excess Heat Production in Bulk Pd Cathodes Electrolytically Loaded with D:

- Maintain High Average D/Pd Ratio (Loading)
- For times $\gg 20-50x \tau_{D/D}$ (Initiation)
- At electrolytic $i > 250-500 \text{mA cm}^{-2}$ (Activation)
- With imposed D Flux (Disequilibrium)

For 1mm dia. Pd wire cathodes:

- $P_{XS} = M (x-x^{\circ})^2 (i-i^{\circ}) \partial x / \partial t$

- $x^{\circ} = 0.84-0.88, i^{\circ} = 350-425 \text{mA cm}^{-2}, t^{\circ} > 200 \tau_{D/D}$

Hypothesis 2

“The observed excess heat originates in a hitherto unexpected and presently unexplained Nuclear Effect and that is a property of Crystalline Metals strongly loaded with Deuterium.”

Experiments:

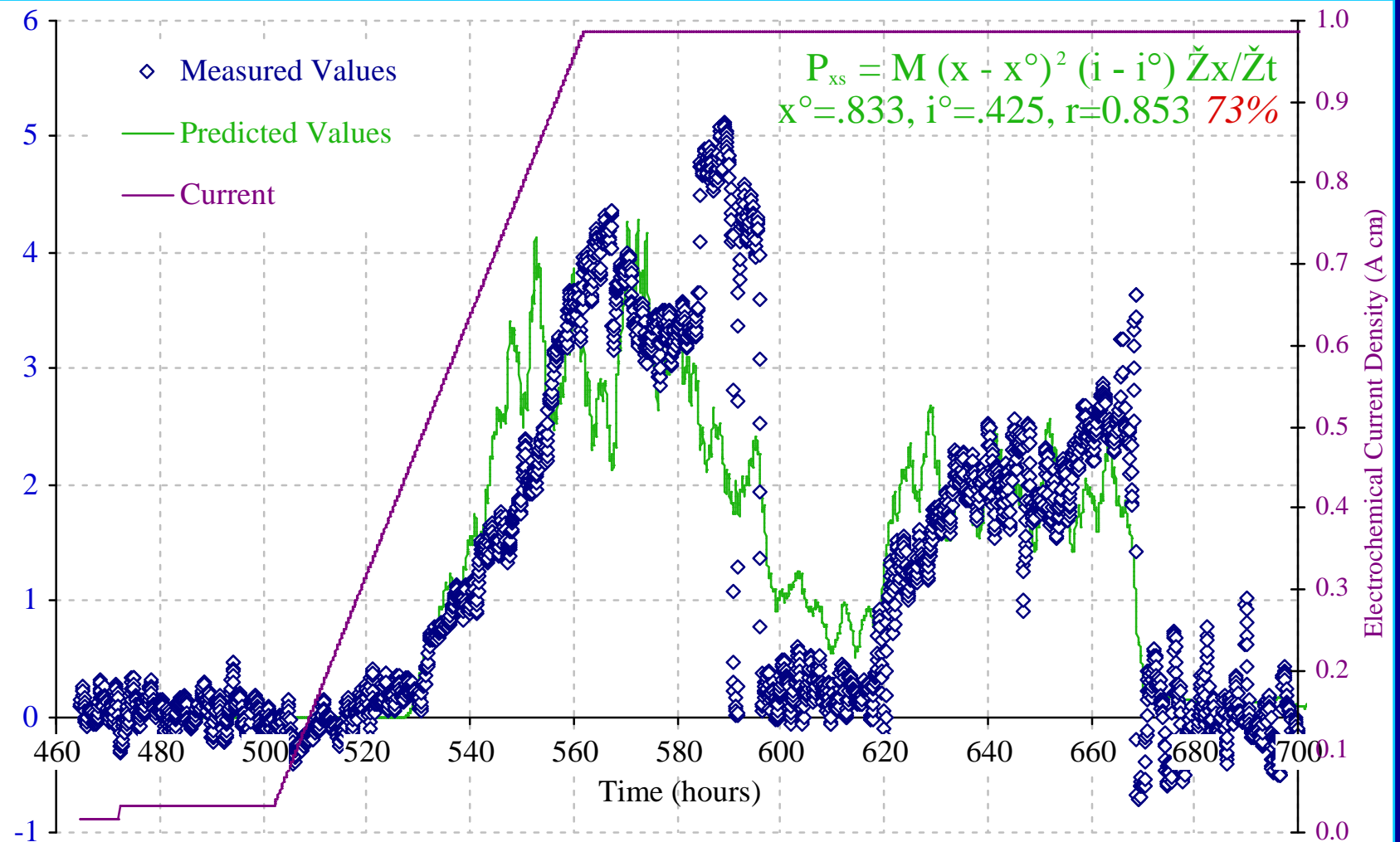
- 2π , real time, “*in situ*” X-ray detector (Lockheed)
- Gamma and X-ray spectrometer (K. Wolf)
- Neutron spectrometer (K. Wolf)
- Charged particles: α , β , p^+ (MIT)
- Tritium
- Helium: ^3He and ^4He (Amarillo, PNNL & Clarke)

Results:

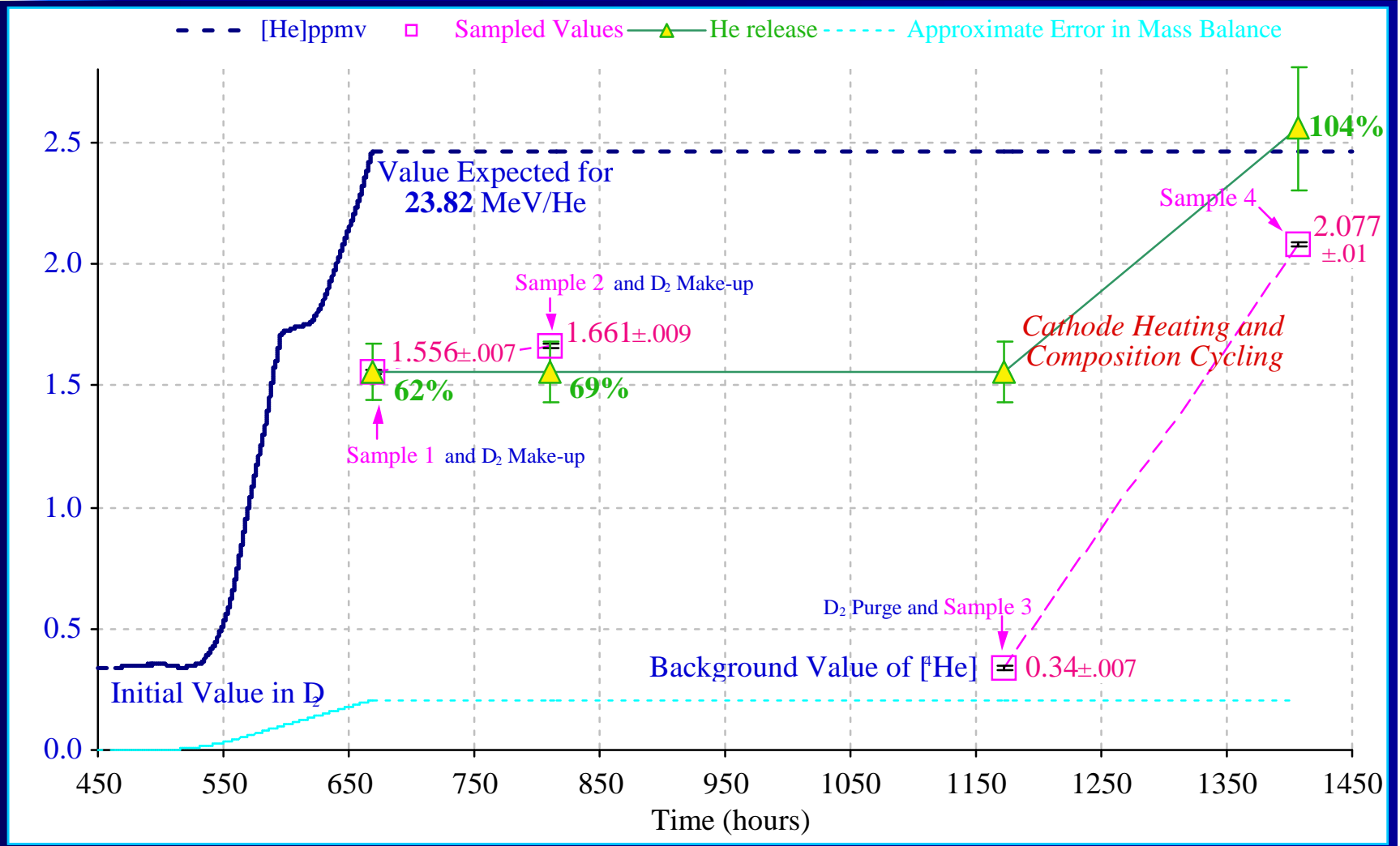
- Correlated heat and ^4He .
- Evidence of Tritium. _____

M4: Excess Power Correlation function

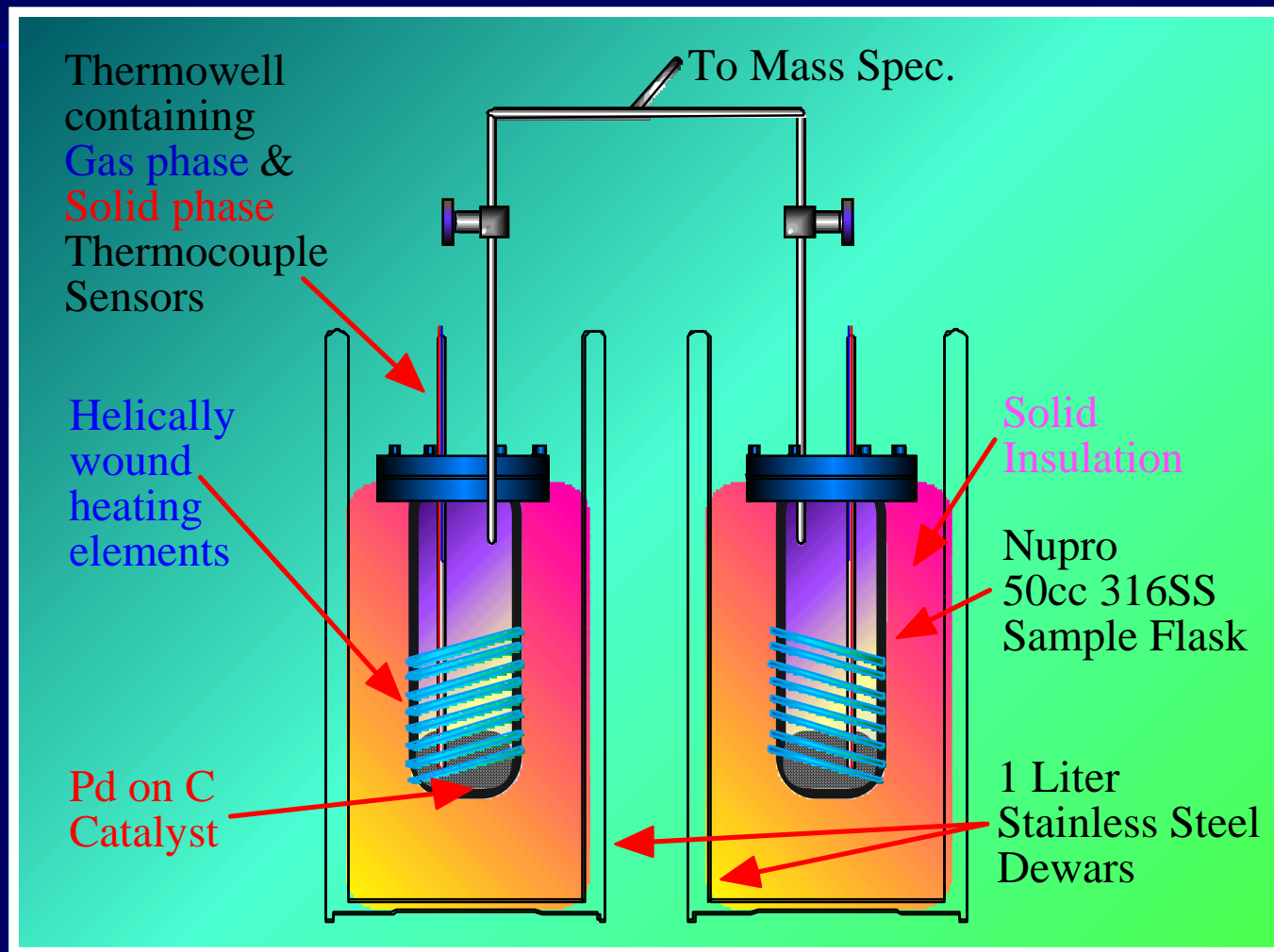
[Closed, He-leak tight, Mass-Flow Calorimeter, Accuracy $\pm 0.35\%$]



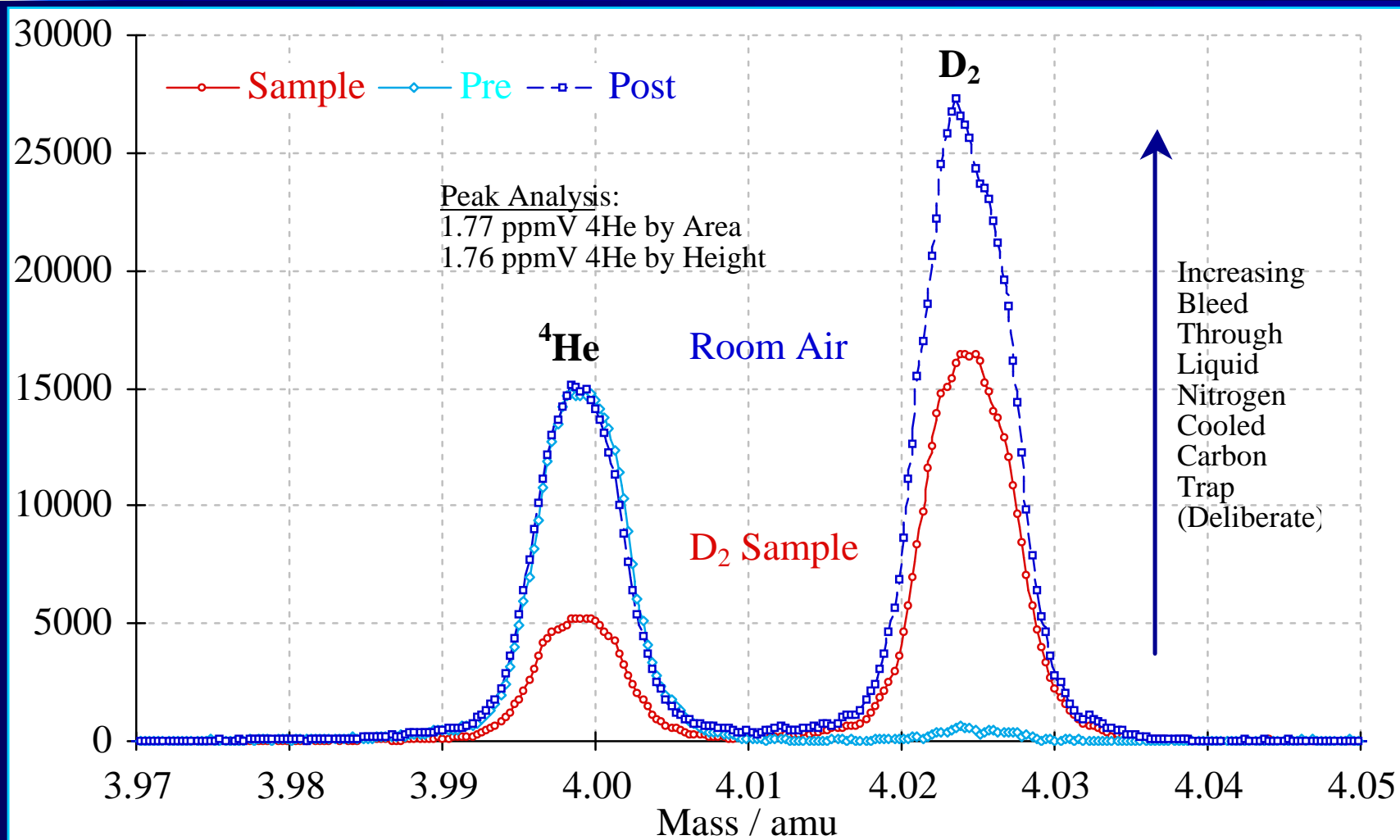
M4: Correlation of Heat with Helium



Case cell Studies: D₂ Gas with Pd/C Catalyst



Extrel QMS: resolution of D_2 & 4He



SRI Micro-Mass 5400 Noble Gas Mass Spectrometer

Specifications:

- Magnetic Sector Analyzer with 90° extended geometry ion optics giving a dispersion length of 54cm

- Helium Sensitivity

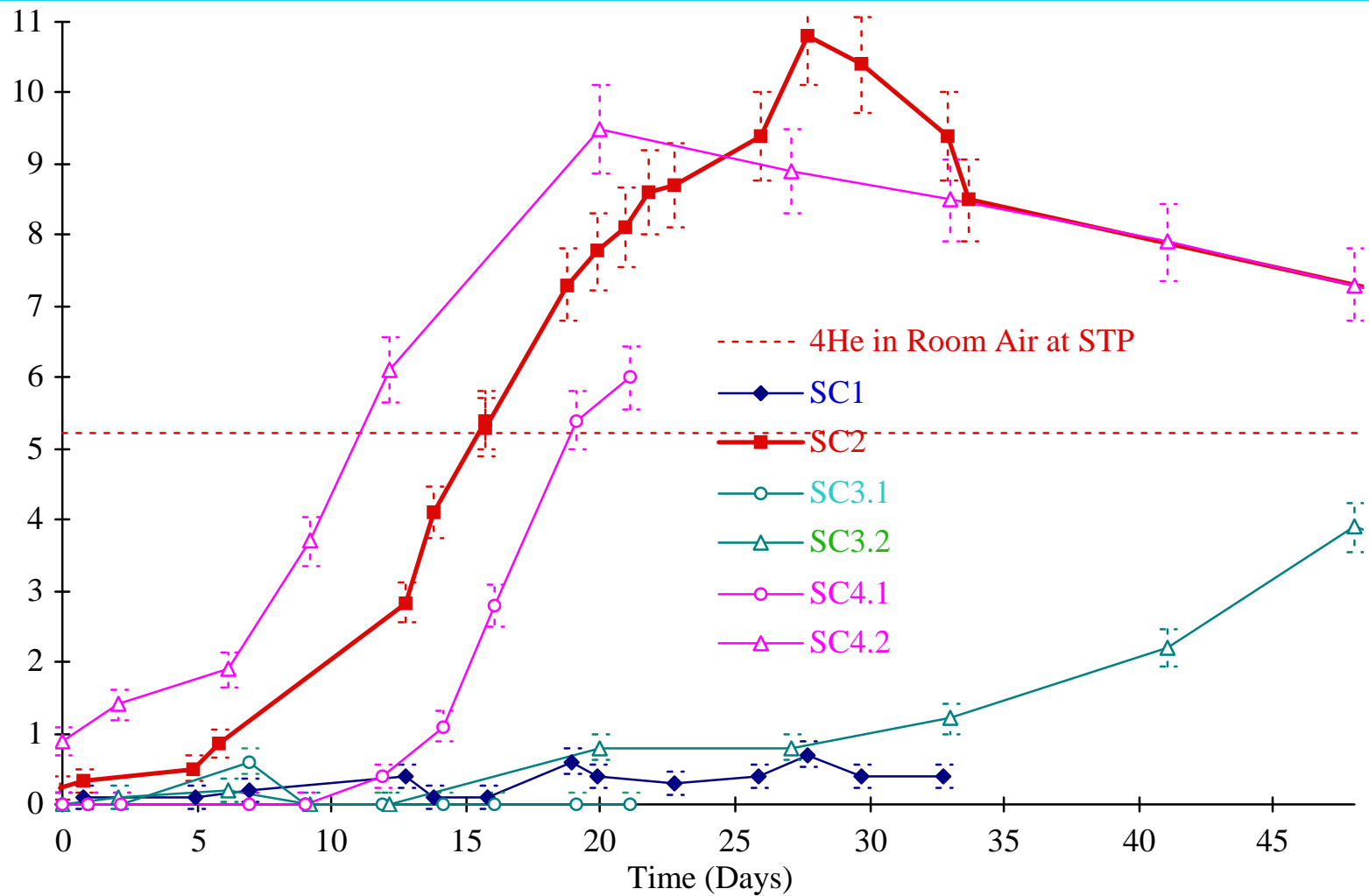
<u>Isotope</u>	<u>Faraday</u>	<u>Channeltron</u>	<u>Absolute resolution</u>
⁴ He	3ppb	2.0pptr	1.0x10 ⁷ atoms*
³ He	3ppb	0.05pptr	2.5x10 ⁵ atoms**

* Limited by background

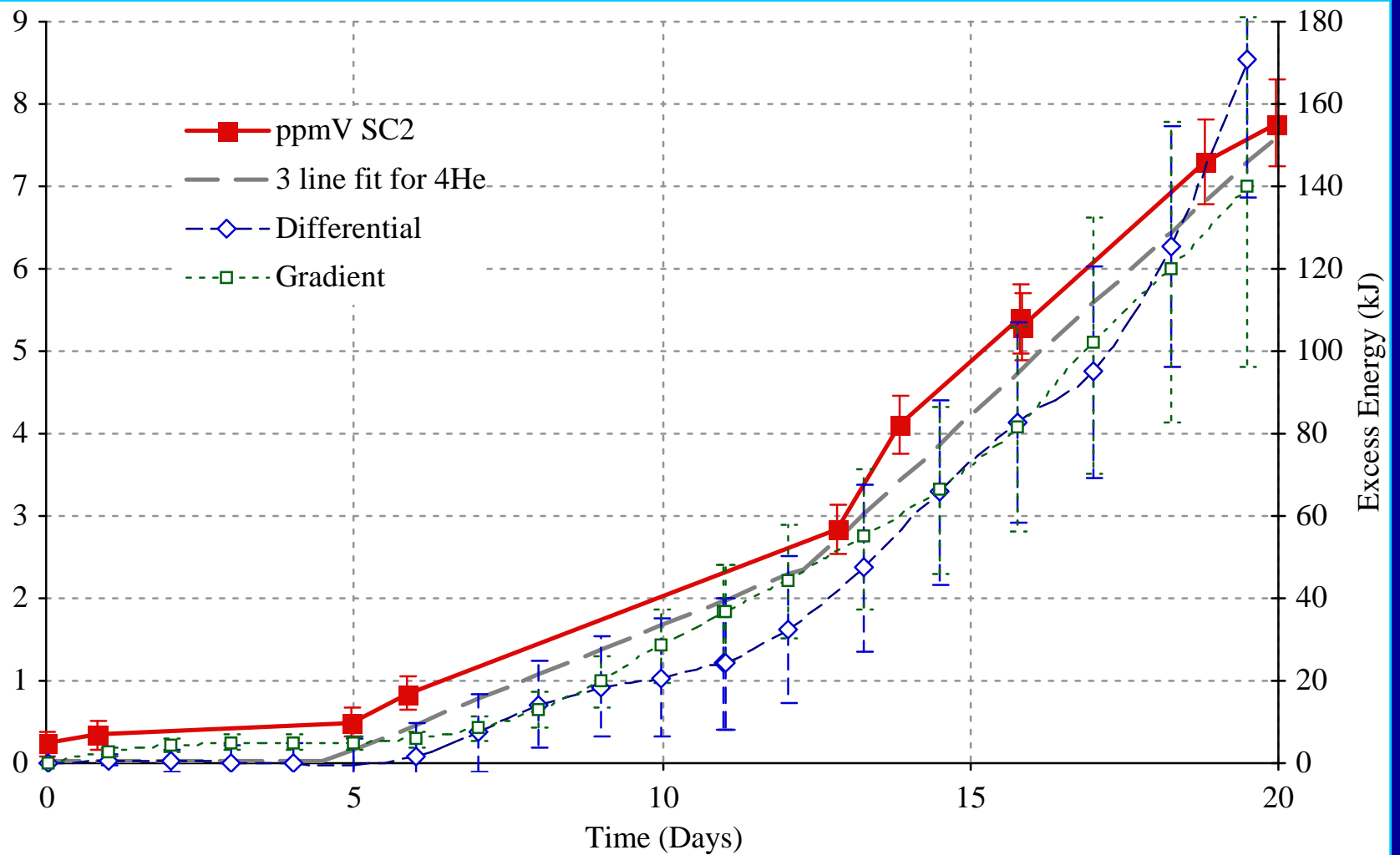
** May be reduced using different method

- Metal Analyses
- still under development

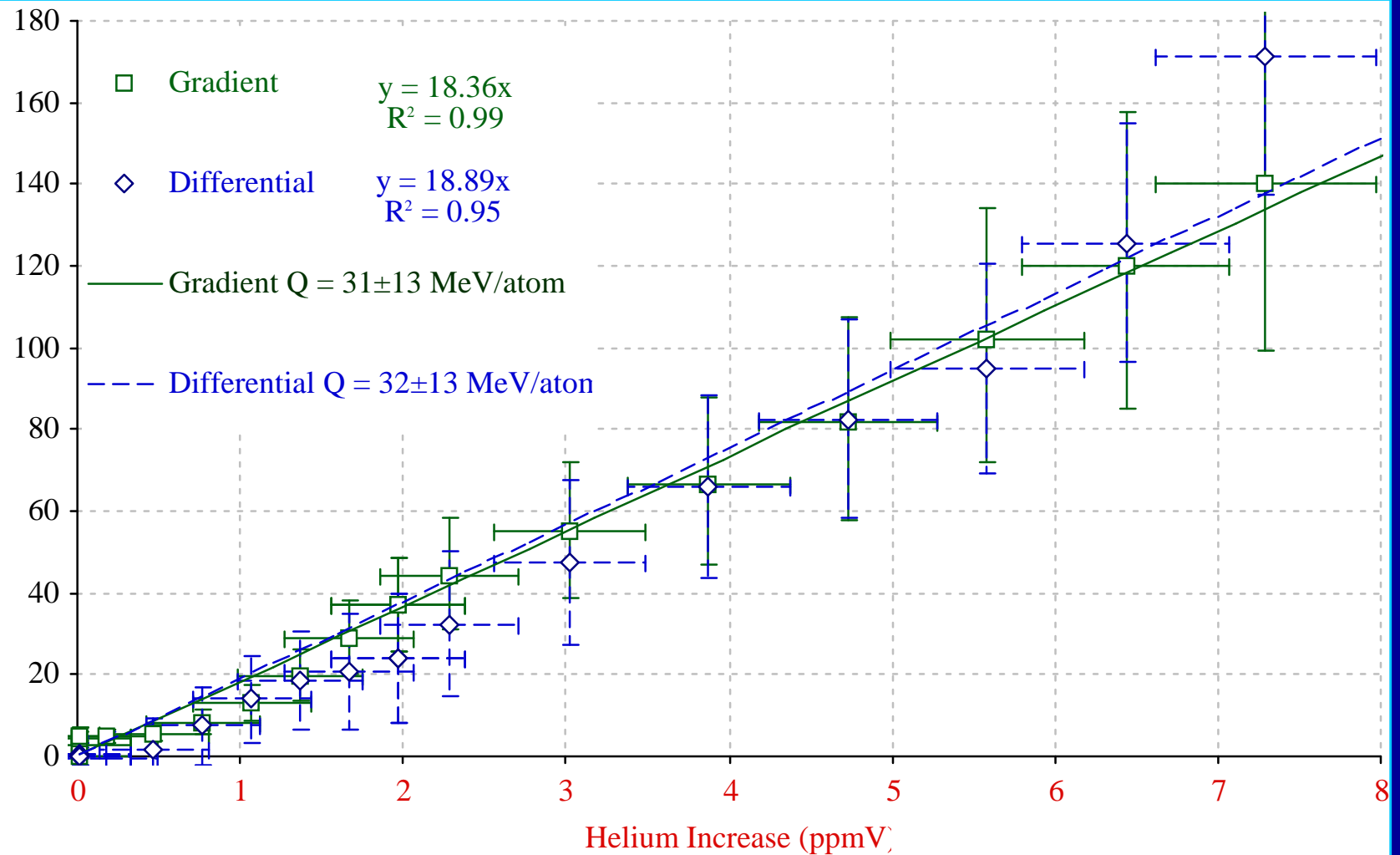
Case: ^4He vs. time



Case: ^4He and Heat vs. time



Case: "Q"-Value - Energy vs. ^4He



Case Conclusions

- Near quantitative correlation between Heat and ^4He production according to:

Predicted: $d + d \rightarrow ^4\text{He} + \sim 24\text{MeV}_{(lattice)}$

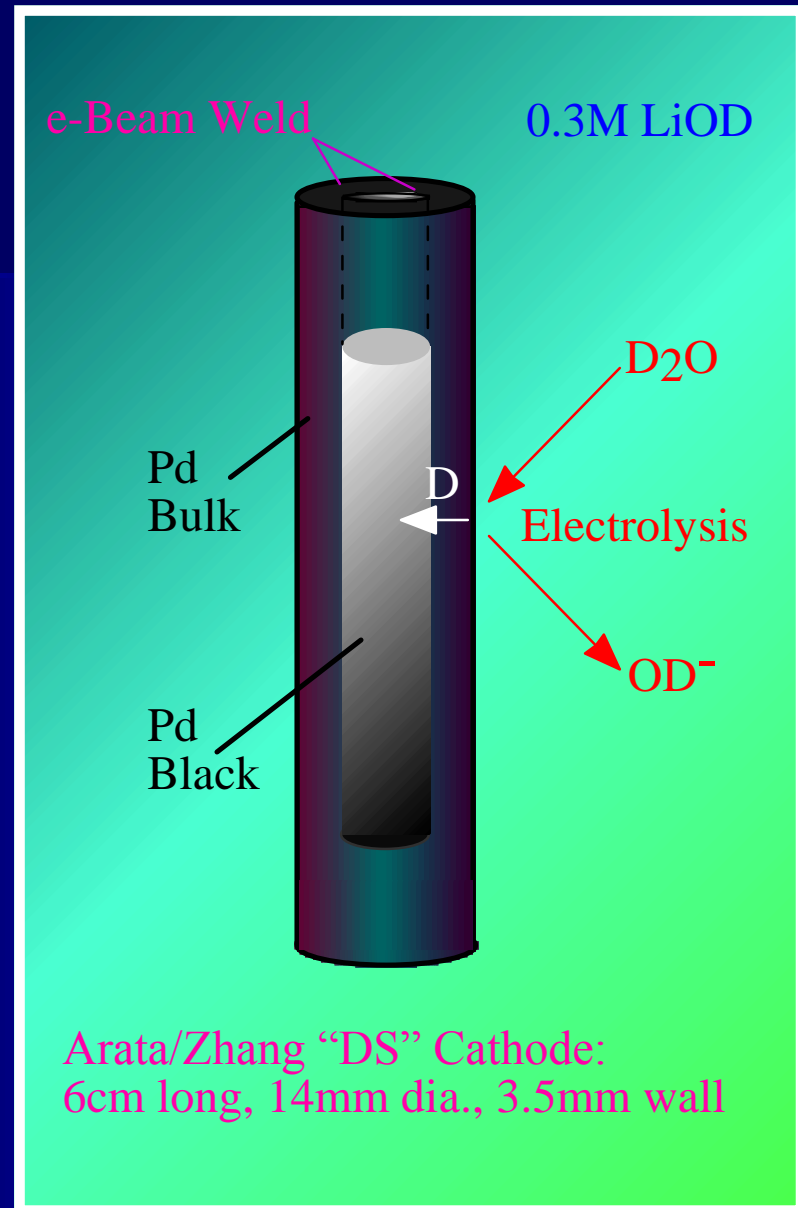
Measured: $Q = 31 \pm 13 \text{ MeV/atom}$

- Discrepancy may be due to solid phase retention of ^4He
- Substantial initiation time \gg D diffusion.
- $\text{Max } [^4\text{He}]_{\text{Sample}} / [^4\text{He}]_{\text{Air}} > 2$

Production of Tritium in a Sealed Pd cavity

AZ1 0.3M LiOD, AZ2 0.3M LiOH
Cathodic Current 5 - 7.5A
Current Density 170-255mA cm⁻²
P_{in} 50-317 W, Duration 120 Days
P_{xs,Max} = 10 ±1.5%, P_{xs} 0 ±1.5%,

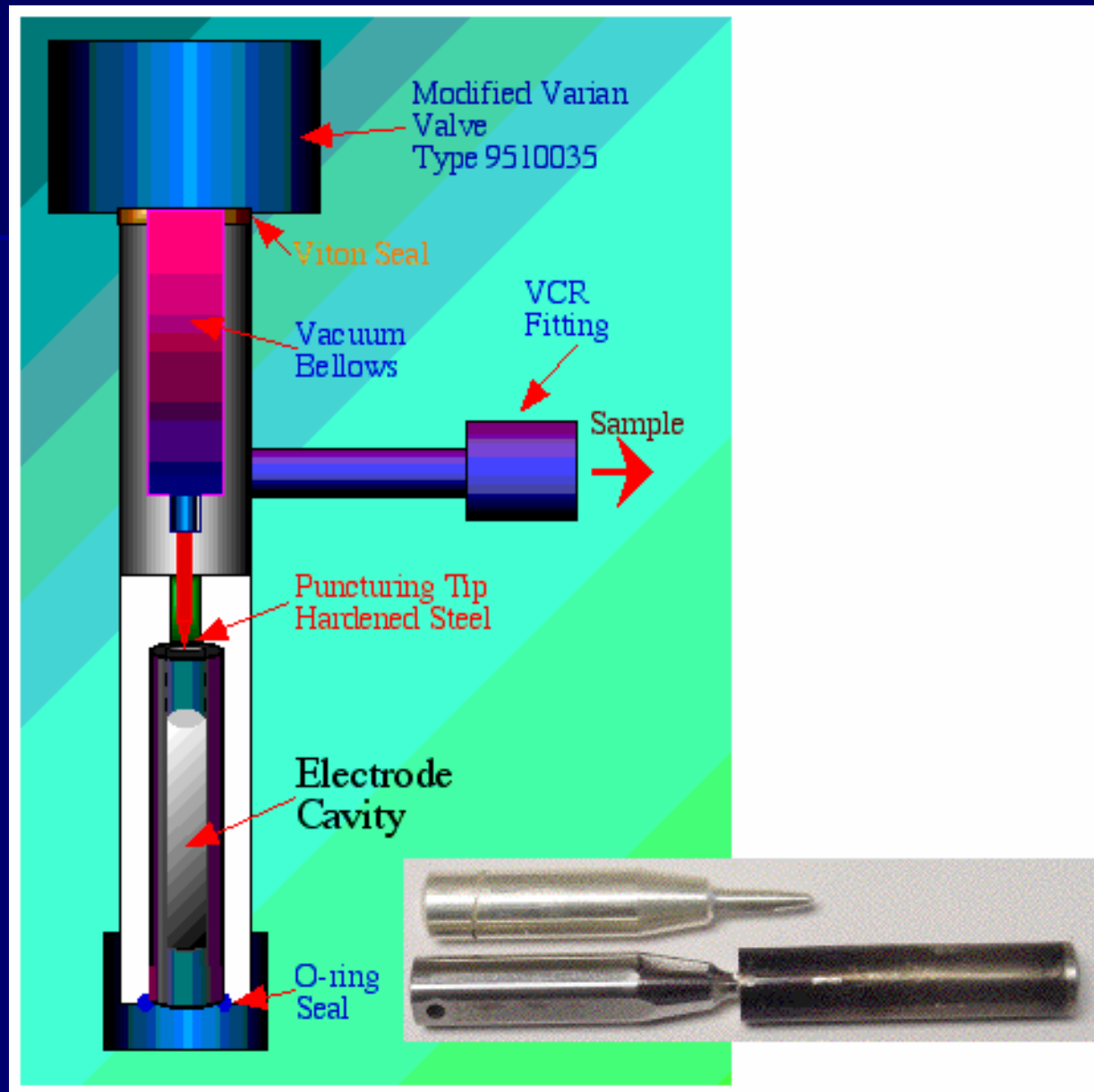
Deloaded:
open circuit and at 2V Anodic
for a further 100 Days.





Gas Sampling Method for Sealed Cathodes

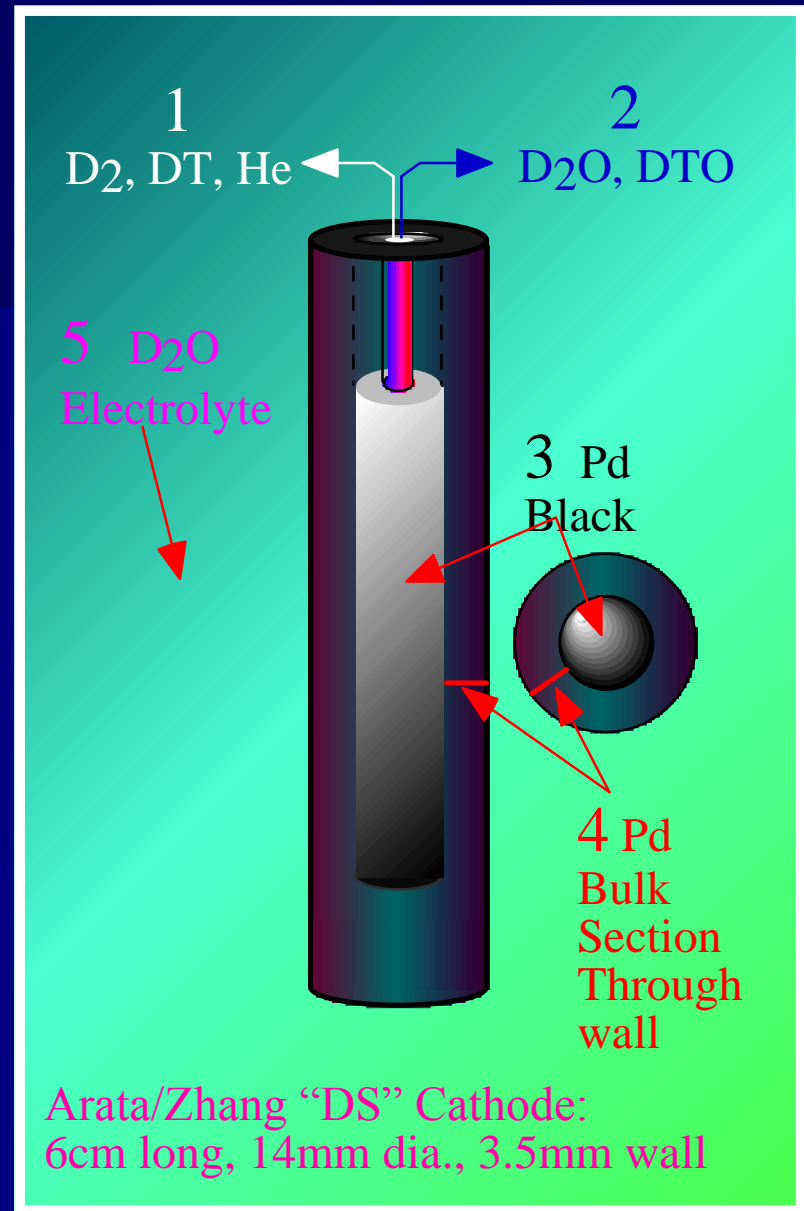
[B. Oliver, PNNL,
analyses performed by:
B. Oliver, PNNL,
W. B. Clarke,
McMaster, Ontario,
and by
V. Violante, ENEA]



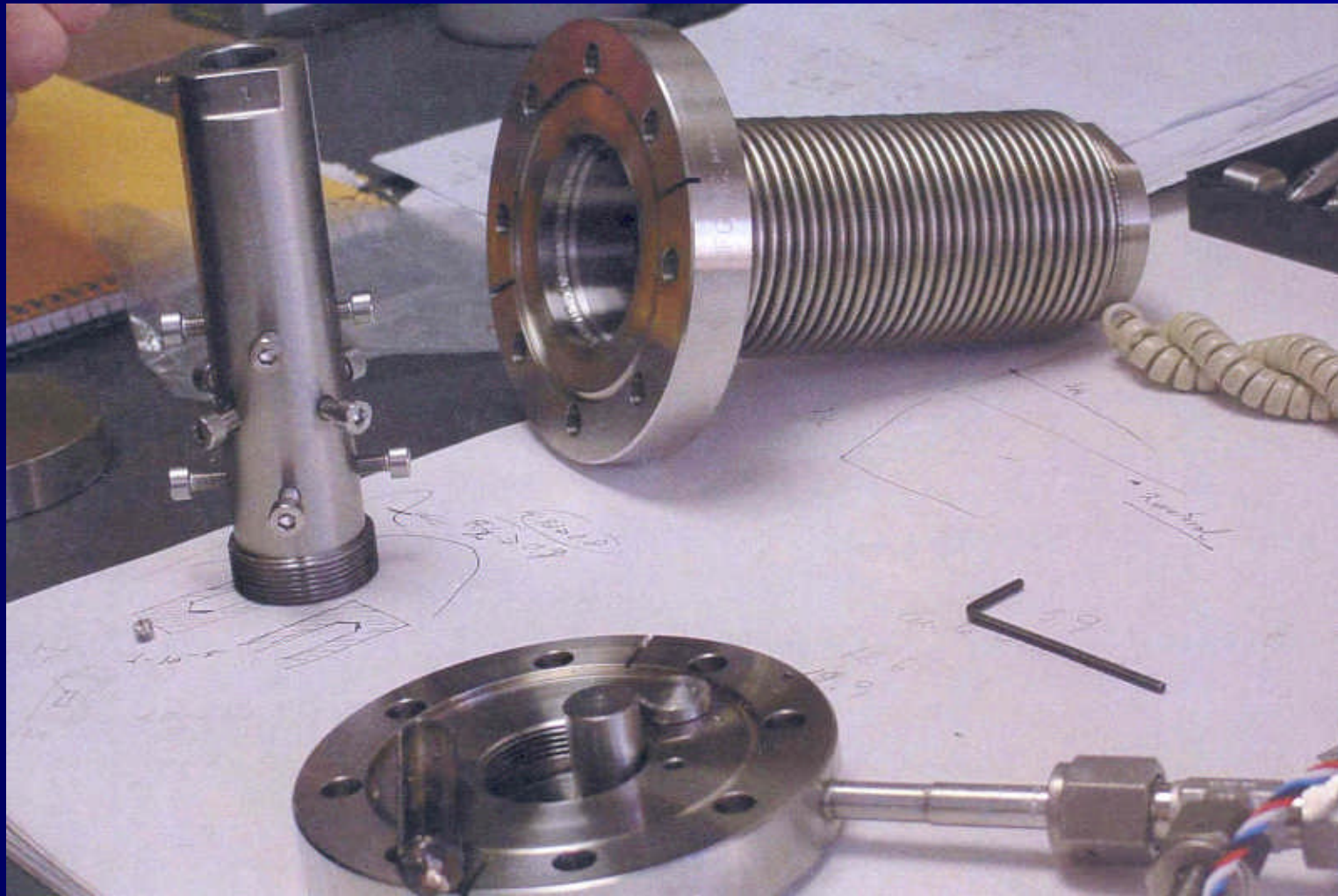
AZ1:
Measurements
of ^3He and ^3H

**T measured as $\partial^3\text{He}/\partial t$ at
McMaster in Phases 1-4**

**T measured by
scintillation at SRI
in electrolyte (Phase 5)**



ENEA/AZ1: Apparatus for Gas sampling in sealed cathode Void



ENEA/AZ1: Press and Bellows



ENE/AZ1: Puncturing tip and cathode



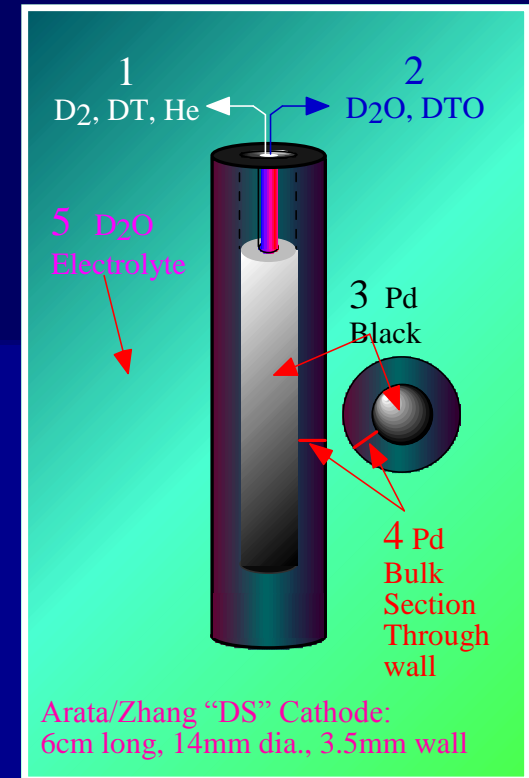
Tip and Cathode

QuickTime™ and a
Photo - JPEG decompressor
are needed to see this picture.

AZ1: Tritium Results

- If Tritium was injected in a single event, this event occurred sometime during the period of cathodic electrolysis.

The total production of Tritium was between 2×10^{15} and 5×10^{15} atoms.



Tritium Fractionates between the 5 Phases as follows:

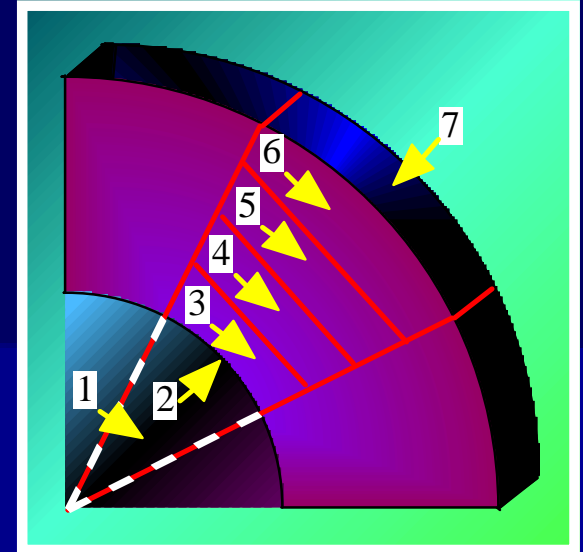
1	2	3	4	5
1.8%	97.8%	0.16%	0.24%	0.05%

Clarke, Oliver, McKubre *et al*, *Fusion Science and Technology*, Sept. (2001)

AZ1: Radial Distribution of ^3He and ^3H :

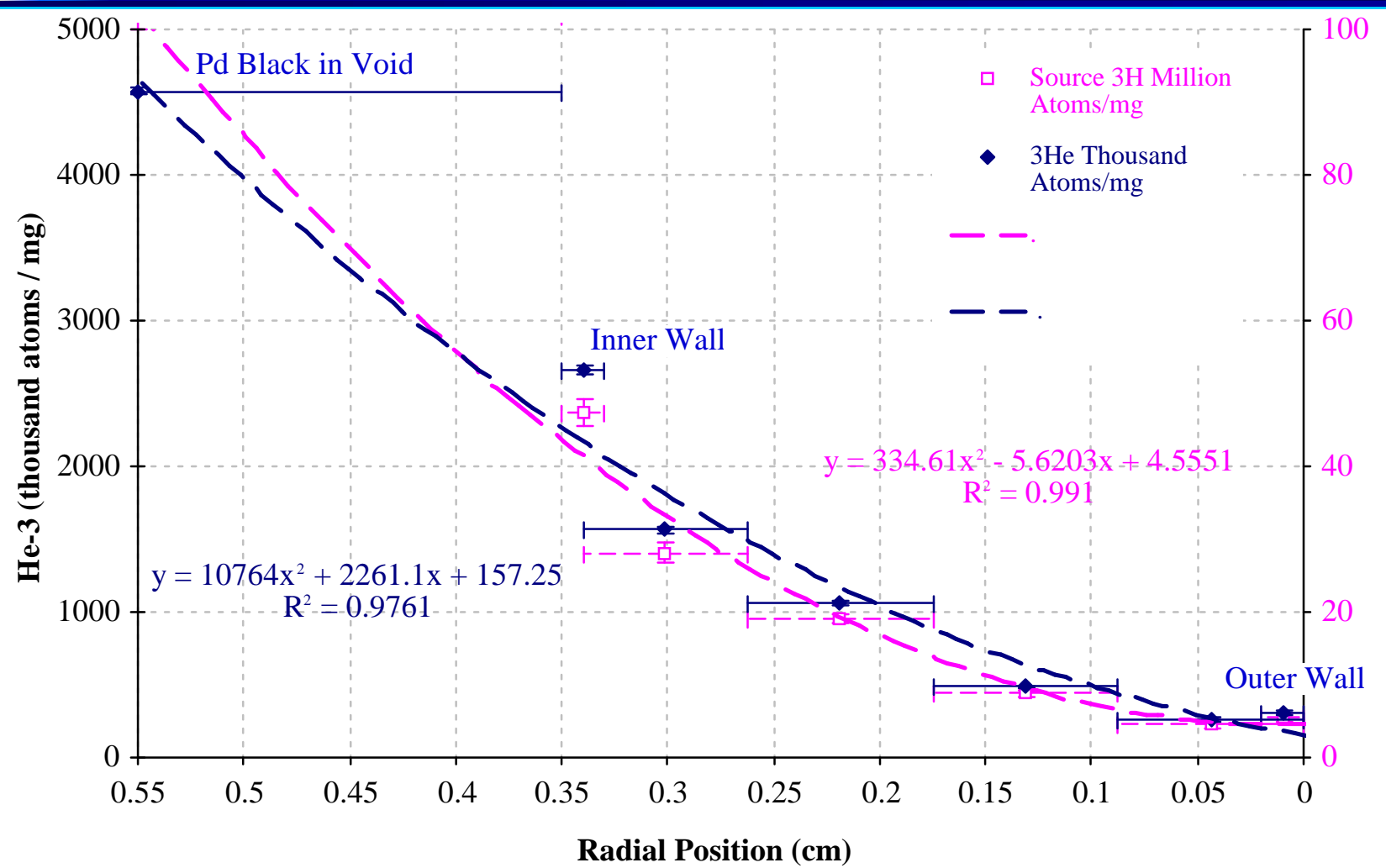
Radial Position (cm)

**[^3He] Thousands of
Atoms/mg Pd**



1	2	3	4	5	6	7
Inside Black	Inner Wall	Inside Black	Inside Black	Inside Black	Inside Black	Outer Wall
0.525	0.345	0.301	0.219	0.131	0.044	0.005
±	±	±	±	±	±	±
0.175	0.005	0.039	0.044	0.044	0.044	0.005
4573	2656	1563	1061	486	261	307
±	±	±	±	±	±	±
21	30	21	11	9	9	10

AZ1: Radial Distribution of ^3He and ^3H



Tritium Conclusions

- Production of Tritium was between 2×10^{15} and 5×10^{15} atoms.

Modeled as a single event, this occurred during cathodic electrolysis.

There is definite evidence of excess ^3He from Tritium decay of all samples of Pd & Pd-black from the D_2O experiment.

Samples of Pd taken from a similar and contemporaneous H_2O electrode show low ^3He levels consistent with blank Pd.

Measurements of the ^3He gradient through the 3.5mm wall of the D_2O electrode show that the ^3He is the decay product of Tritium which diffused from a source inside the electrode.

No evidence for ^4He quantitatively consistent with excess heat.

Summary and Conclusions (1)

Experience teaches us that:

(1) There ARE heat effects closely correlated to the Loading:

- Stoichiometry of D/Pd
- Chemical Potential of D?
- New Phase formation?

Initiation:

- Lattice defects (vacancies and impurities)

Stimulation:

- Electromagnetic, Acoustic, Magnetic.....
- Flux effects (D^+ , e^-)

Summary and Conclusions (2)

Experience teaches us that:

(2) There ARE (hitherto unexpected) nuclear effects:



- 3 metal-sealed cells
- 3 calorimetric methods
- electrochemical and gas loading experiments
- ${}^4\text{He}$ analyses at 4 different institutions

${}^3\text{H}$ production in small dimension Pd particles

Numerous other effects

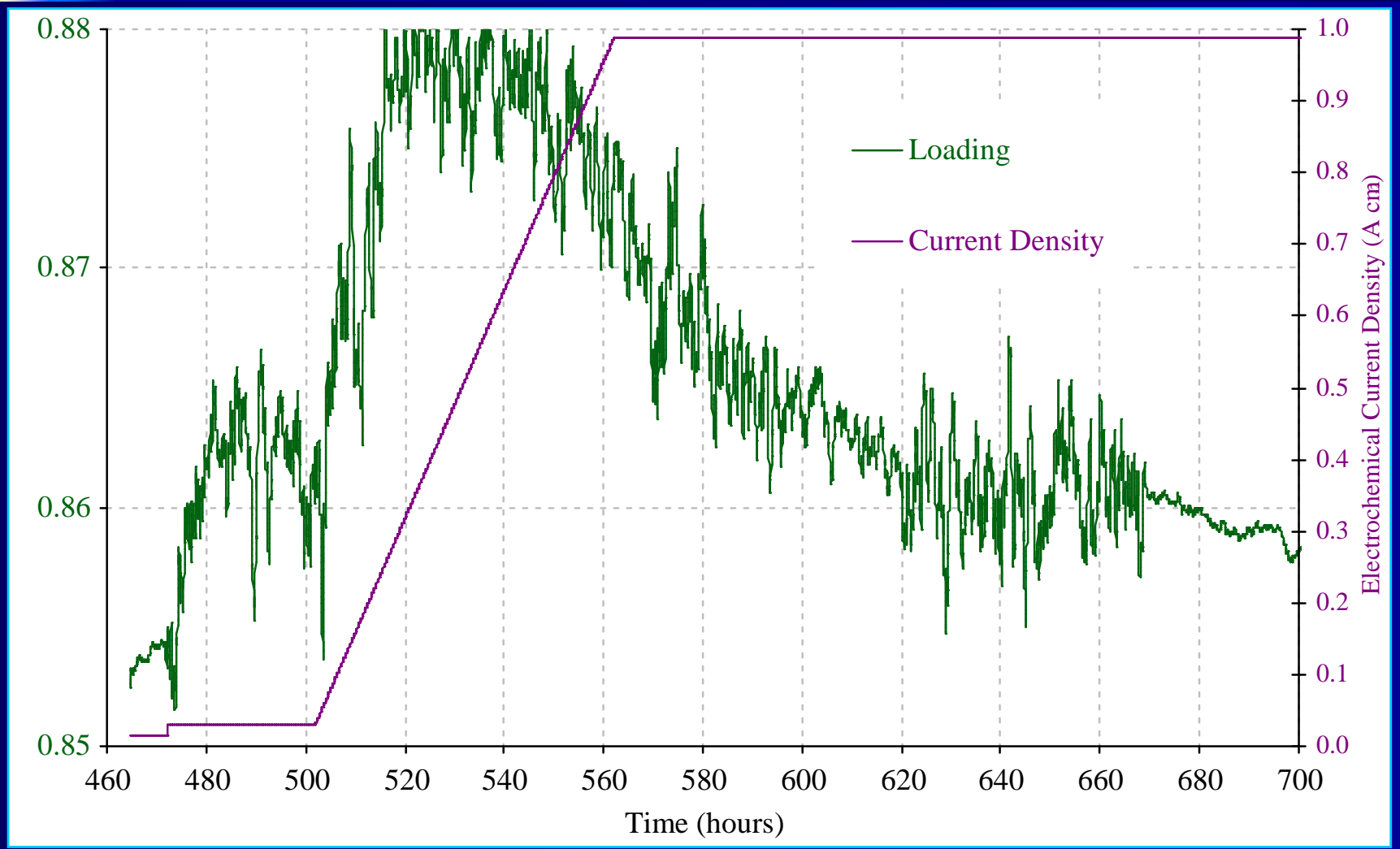
Summary and Conclusions (3)

Experience teaches us that:

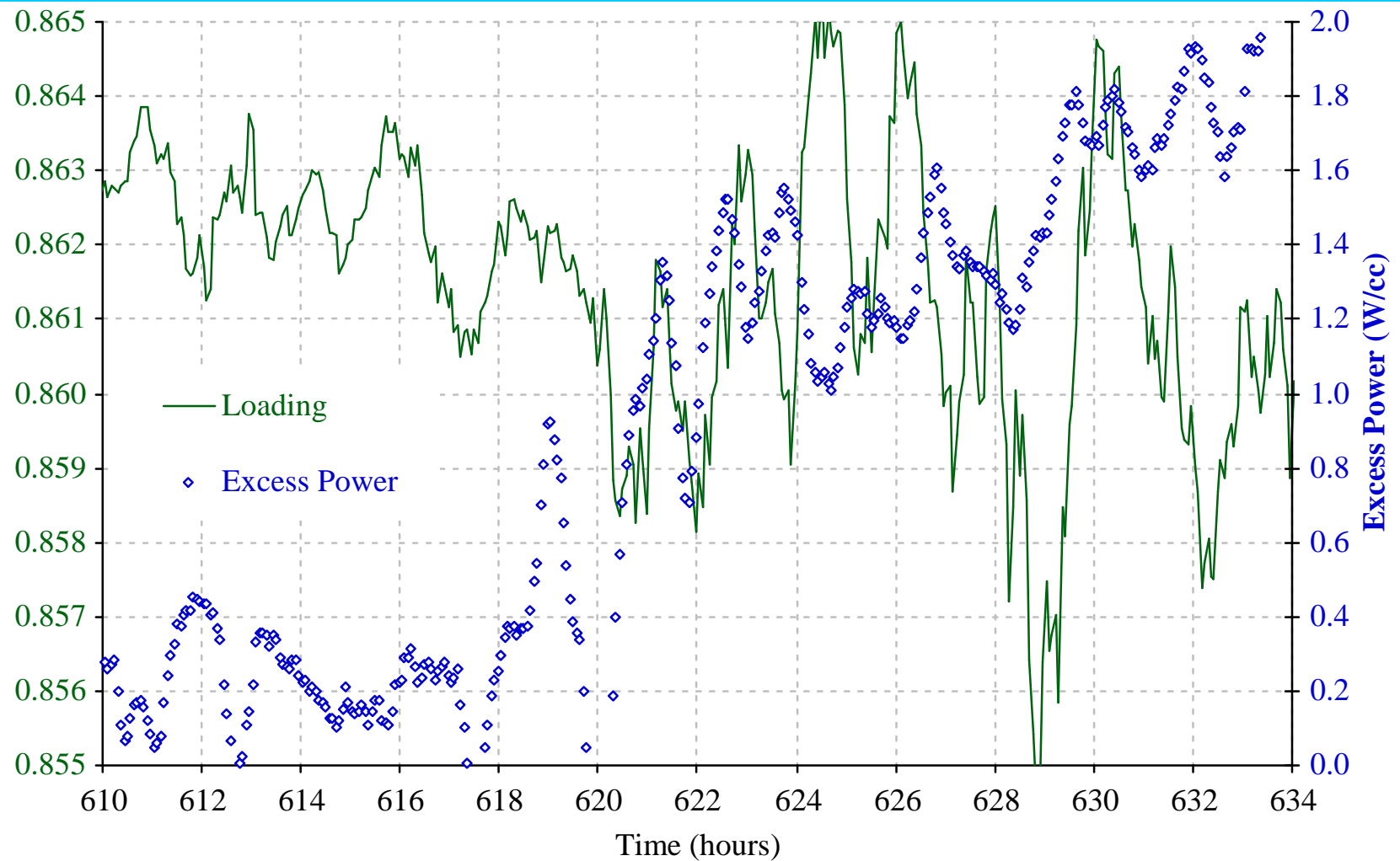
(3) Effects ARE amenable to conventional interpretation.

Backup Slides

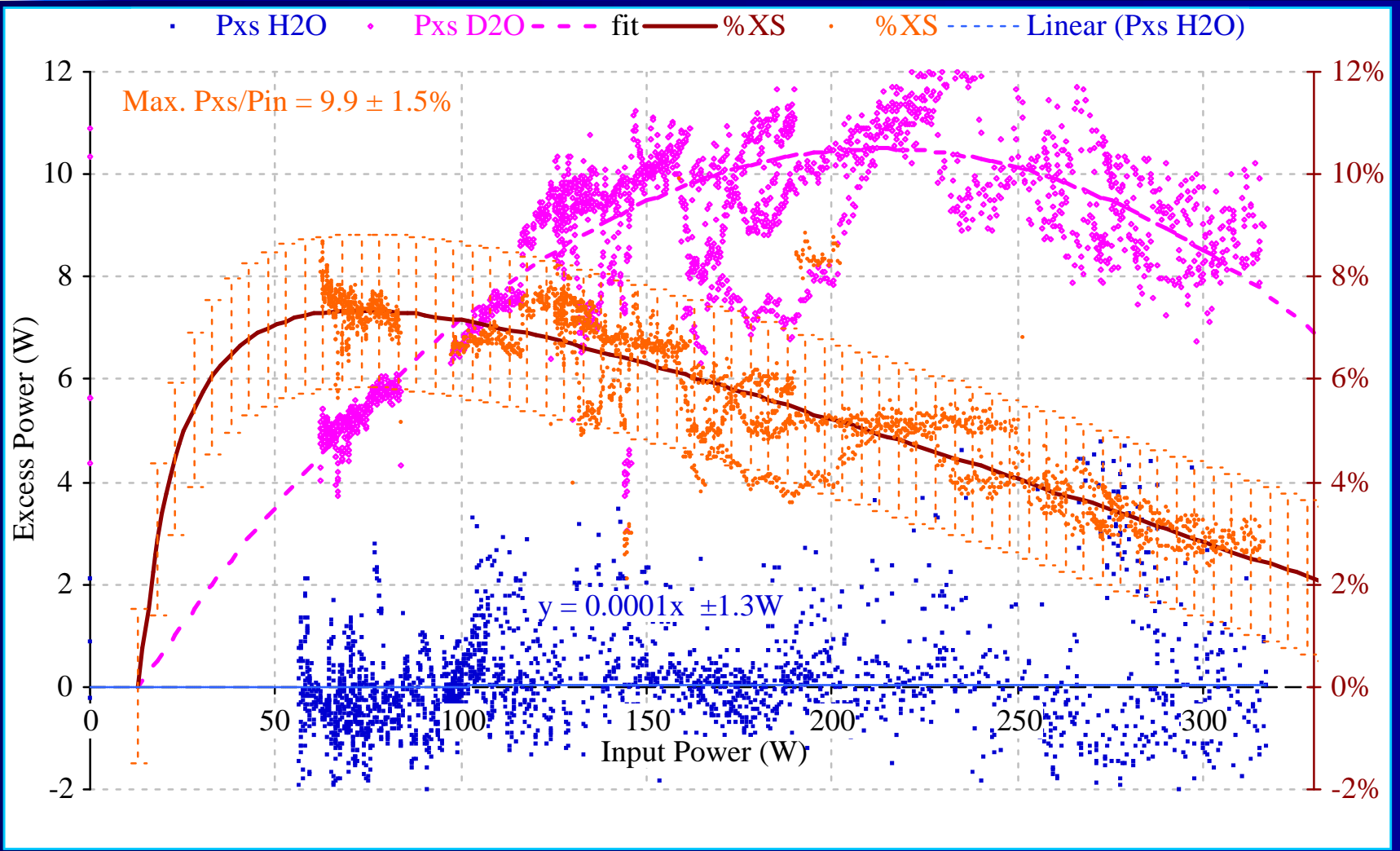
M4: The Dynamics of D Flux



M4: The Dynamics of Flux (*detail*)



AZ1,2: P_{XS} vs. P_{in}



The Pathway Forward:

- Predictive Theory

- After 14 Years of Parametric Study we have learned a great deal // intuition and patience is thin

- Simple demonstration of a novel effect having an unambiguously nuclear origin:

- Results are too numerous (>3000 papers) incomplete, complicated, unexpected require multi-disciplinary understanding
- Results sufficiently substantial to allow evaluation of potential technological consequences.
- Capable of independent replication.

Flow Calorimetry Details (1)

1. Operate calorimeter in constant power mode by adjusting electrochemical power and calibration heater power to be a constant sum. This maintains the calorimeter in near steady state condition.
2. Temperature sensors initially two RTD's at inlet and outlet, later two RTD's and two thermistors at the outlet.
RTD sensitivity ± 1 mK
Thermistor sensitivity ± 50 μ K
3. Flow Rate Measurement on-line, gravimetric and volumetric

Flow Calorimetry Details (2)

4. Heat Transfer Fluid

Silicone oil: low C_p , insulating, non-corrosive
absorbs water (viscosity, C_p)

Water: lower viscosity, C_p constant and
well determined

All connections and wire feed throughs designed to eliminate heat transfer fluid leaks.

5. All connections and wire feed throughs designed to eliminate heat transfer fluid leaks.

6. Fluid streamlining reduced by thorough mixing of exit stream.

Flow Calorimetry Details (3)

7. Electrical leads brought in through bottom of calorimeter to reduce heat transfer along the wires (**later labyrinth design**).
8. Calorimeter held in constant temperature bath to minimize cooling losses and maintain them constant, also to maintain constant inlet temperature.
9. Calorimetric parameters measured via computer controlled multiplexer using a single calibrated DMM (periodically interchanged).
10. Series cell operation

SRI Micro-Mass 5400 Noble Gas Mass Spectrometer

